

Phytoremediation: Carbon Dioxide (CO₂) and Nutrient Removals by Aquatic Plant Treatment System (APTS)

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The experiments were conducted to investigate the removal of nitrogen (N), phosphorus (P) and carbon dioxide (CO₂) by four selected plants. The plants were cultured in phyto-reactor. The reactors were examined by batch operation under certain light intensity and temperature. Results showed that more than 80% of nitrate as nitrogen (NO₃-N) can be removed for all phyto-reactors contained aquatic plants; only 35% of NO₃-N was removed by control reactor. Phosphate as phosphorus (PO₄-P) removal was 86% for control reactor and 90-96% for phyto-reactors contained aquatic plants. Increase of elevated CO₂ 500-2,000 ppm enhances the CO₂ removal rate by those aquatic plants. More than 95% of CO₂ were removed by aquatic plants at elevated CO₂ of 2,000 ppm. No significant changes of CO₂ were observed by control reactor at every elevated CO₂ concentrations.

Key words : Aquatic Plant Treatment, Nutrient Removals, CO₂ Sequestration and Plant Species

1. Background

The rapid growth of industry and major agricultural activities to supply the human consumptions causes a destruction of ecosystems and addition of air and water pollutions. Excess nutrients resulted from discharge of untreated wastewater to water resources led to eutrophication phenomena. In addition, the role of carbon dioxide (CO₂) in climate changes is one of the most important environmental issues. Higher concentrations of CO₂ and other greenhouse gasses (GHG) reduce the ability of the Earth to radiate planetary heat through the atmosphere. Most scientists agree that the increase of CO₂ is a major cause in the observed trend of global climate warming¹⁾. It is therefore necessary to have available technology which minimizes the discharge of CO₂ into the atmosphere. One ecological method to treat polluted water contained high nutrients and to reduce the increase of CO₂ levels in the atmosphere is aquatic plant treatment systems (APTS). APTSs are treatment systems that combine physical, chemical, and biological processes in an engineered and

managed system. In aquatic plant systems, wastewater contained excess nutrients are treated principally by means of plant-bacterial metabolism and physical sedimentation process. Photosynthesis process withdraws CO₂ from the atmosphere by photosynthesis process. Carbon sequestered from the atmosphere is stored in plant fiber for extended periods of time. High atmospheric CO₂ levels enhanced plant productivity generally and, consequently, the rate at which CO₂ is removed from the atmosphere^{2), 3)}. Successful performance of aquatic plants for the treatment of contaminated water and soil is being clearly acceptable by scientists and engineers. However, the use of phytoremediation for air pollution prevention is only at early stage of commercial and public developments.

2. Methodology

2.1. Design of Phyto-reactor

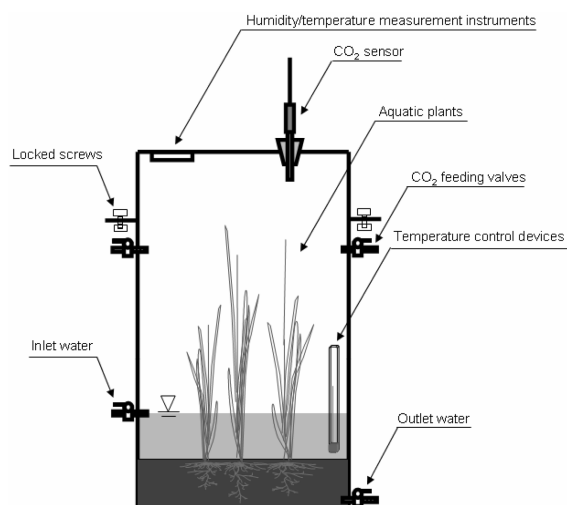
Phyto-batch reactors were made of acrylic and air-tight materials with a dimension of 230 mm × 230 mm × 600 mm. Top of reactor was connected with the CO₂

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Table 1. Raw wastewater characteristics

Parameters	Units	Quantity
pH	-	7.1-7.7
Dissolved Oxygen (DO)	mg O ₂ /L	4.0-5.0
Temperature	°C	25.0
Nitrate Nitrogen (NO ₃ -N)	mg/L	14.0-17.8
Phosphate (PO ₄ ³⁻ -P)	mg/L	14.5-15.7

sensors (probe types) model GMP70 obtained from Vaisala Co., Ltd (Finland). Fig. 1 shows the phyto-reactor used for the experiments. The phyto-reactors were replaced of Ø10-15 mm of gravel and Ø0.6-2.4 mm of sand with approximate depth of 2 cm and 8 cm. Various kinds of aquatic plants; *Cyperus alternifolius*, *Dracaena fragrans*, *Iris ensata*, and *Thalia dealbata* were planted into each phyto-reactor and filled up with 3.5 L of synthetic wastewater (Table 1). Water level of each reactor was remarked. An addition of de-ionized water to phyto-reactor is sometime necessary to maintain constant level of water-table from water loss by evaporation. High concentrated CO₂ gas (99% v/v) was diluted with ambient air and filled to the phyto-reactor by batch operations. The CO₂ concentrations of 500-2,000 ppm are distributed to the phyto-reactors for 8 hr/day. The light source used for the experiment was florescence lamp OSRAM FL40 provided light intensity at the top of PBR-surface by 55 ± 5 mmole/m²/s. The temperature in the phyto-reactors is controlled at 25 °C. The effluent treated wastewater was sampled at the bottom of the phyto-reactors and analyzed for the main nutrient quality parameters such as NO₃-N, NH₄-N, NO₂-N and PO₄³⁻-P by spectrophotometric method. The

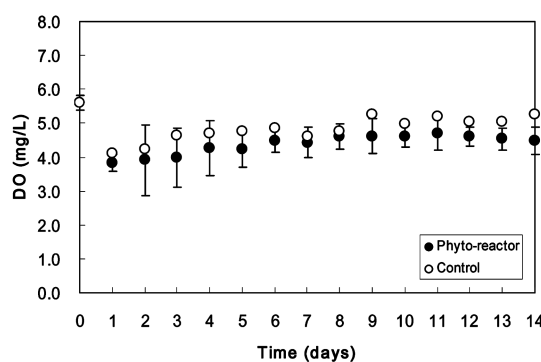
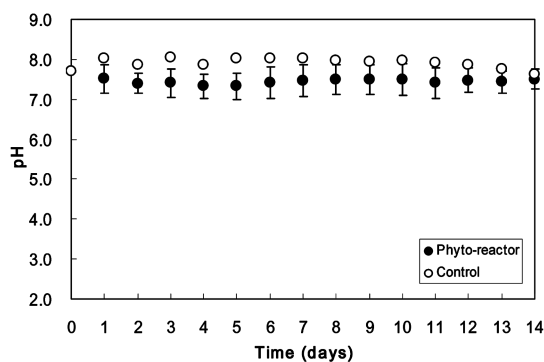
**Fig. 1.** Phyto-reactor.

test-kits used in the experiment were ECOTest obtained TECHCROSS Inc. The wavelengths (l) used by NO₂-N, NO₃-N, NH₄-N and PO₄³⁻-P were 450, 540, 600 and 660 nm. Fig. 2 shows the standard curves for nutrient analysis by ECOTest.

3. Results and discussion

3.1. pH and DO

The temperature was controlled at $25 \pm 0.7^\circ\text{C}$. No significant change of pH was observed in phyto-reactors and control reactor. The pH in phyto-reactors and control reactor was varied from 6.9-7.7 and it trends were increased. Dissolved oxygen (DO) concentration in phyto-reactors was fluctuated from 2.7-5.8 mg/L (Fig.

**Fig. 2.** N and P standard curves.

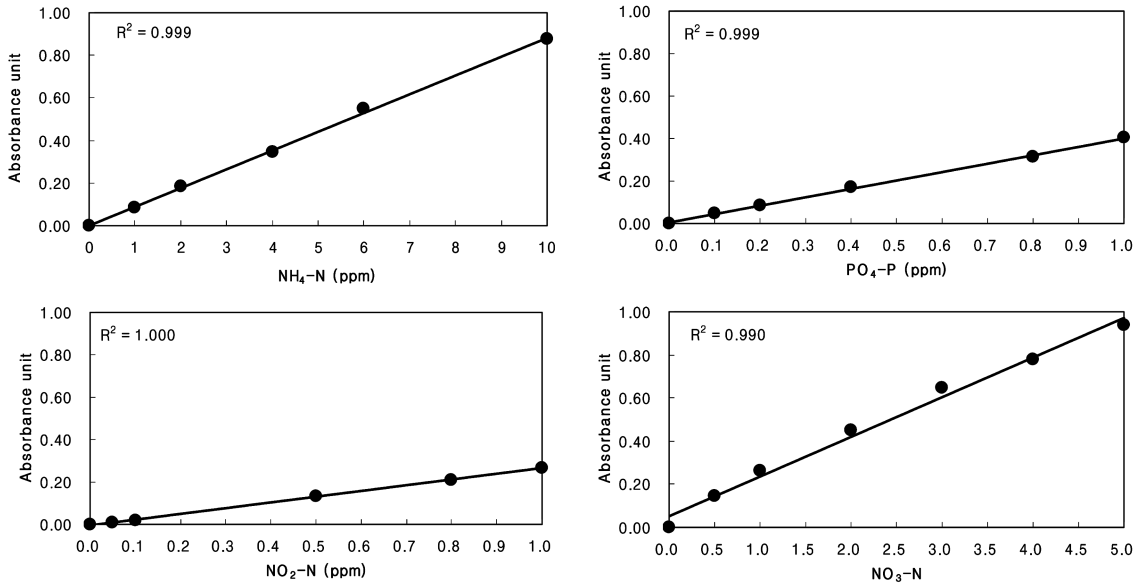


Fig. 3. Variation of pH and DO.

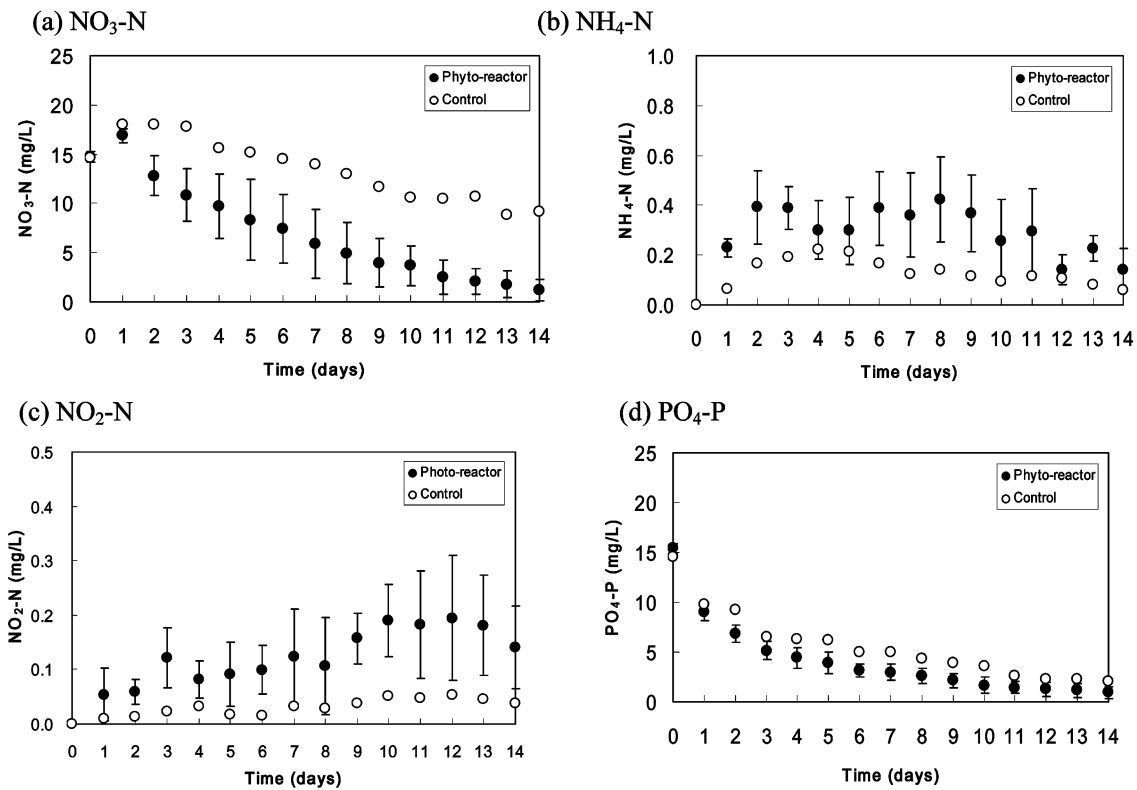


Fig. 4. Variations of nitrogen and phosphorus.

3). Data indicated that rapid reduction of DO in the phyto-reactors was at 1-2 days of the experiments. The

reason might that the depletion of oxygen diffused through the soils under undrained condition and the

remaining of organic matters in media beds coupled with the decaying of some death leaves of aquatic plants in phyto-reactors caused high oxygen demand during 1-2 days of the experiment. After day 3, the DO concentrations in PBRs were enhanced.

3.2. Effect of phyto-reactor on N and P removal

Fig. 4 shows the variation of N and P in the phyto-reactors (The points and bars indicate the average values \pm SD, $n = 4$). The results showed that 86.6%, 80.8%, 95.1% and 96.9% of $\text{NO}_3\text{-N}$ can be removed by phyto-reactors contained *C. alternifolius*, *D. fragrans*, *I. ensata*, and *T. dealbata*. Only 35.1% of $\text{NO}_3\text{-N}$ was removed by control reactor. High $\text{PO}_4\text{-P}$ removal was

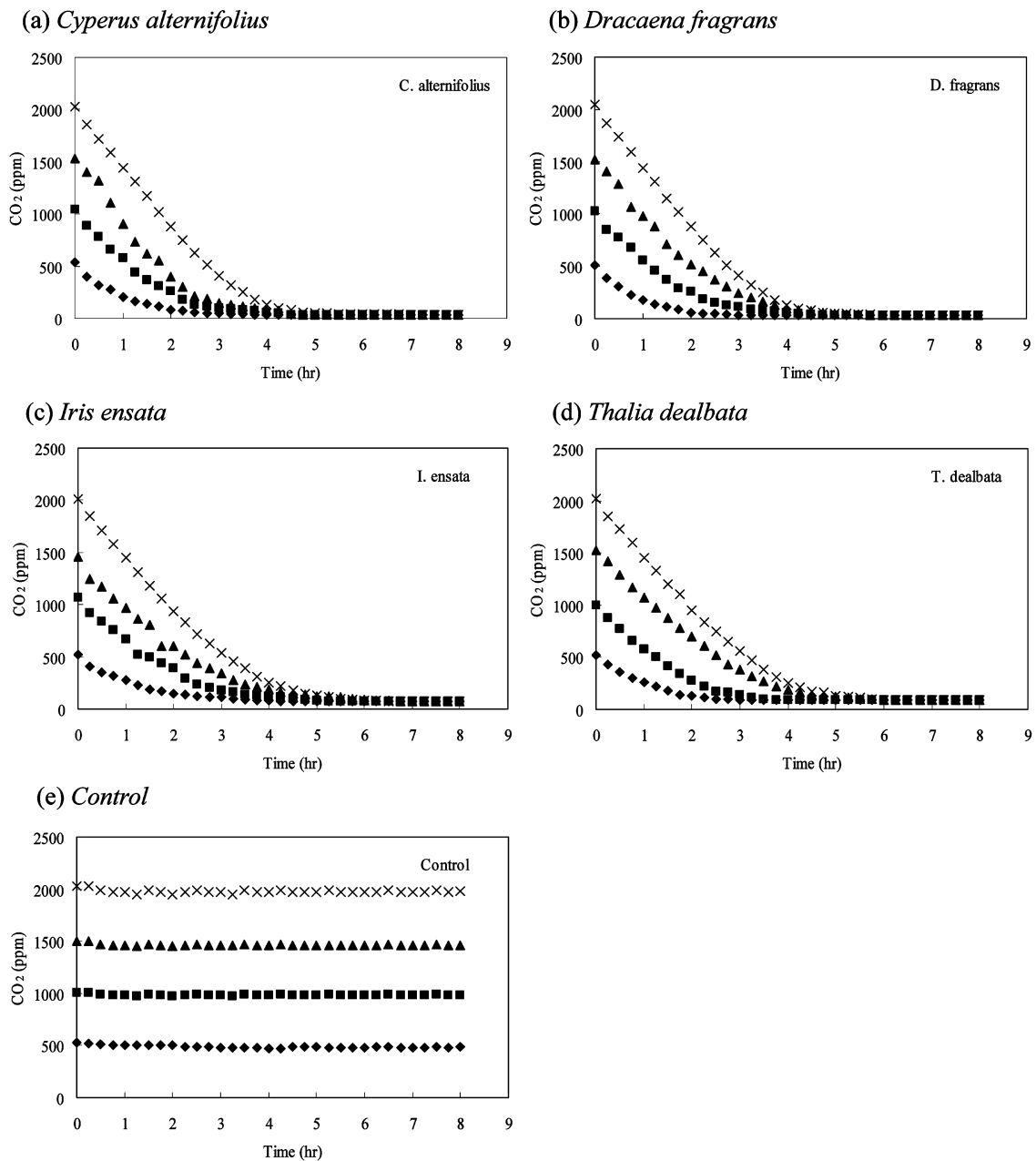


Fig. 5. Variation of CO_2 in phyto-batch reactor.

obtained by phyto-reactors and control reactor. The PO₄-P removal orderly was 86.0%, 96.4%, 90.3%, 90.0% and 98.2% for control and phyto-reactors contained *C. alternifolius*, *D. fragrans*, *I. ensata*, and *T. dealbata*. During the experiments, the NH₄-N and NO₂-N were occurred in the phyto-reactors. NH₄-N concentrations were sharply increased during 2-3 days of the experiments and it was reduced by the end of the experiments, while NO₂-N concentrations were gradually increased during 14 days of the experiments. Several reasons explained the occurrences and changes of NH₄-N and NO₂-N were degradation of plant matters and remaining of organic N in the soils, ammonia volatilization, nitrification and denitrification processes^{4,5)} and physico-chemical properties of media beds used in PBR including chemical adsorption and precipitation on hydrous oxides of Fe, Al, Ca minerals in beds⁶⁻⁸⁾ were included.

3.3. Effect of phyto-reactor on CO₂ Removal

Fig. 5 shows the changes of CO₂ concentrations in the phyto-reactors. The graph illustrated that CO₂ concentrations in phyto-reactors were reduced by time function due to photosynthesis process. At 5 hours of the experiments, CO₂ concentration inside the reactors was less than 100 ppm for every phyto-reactors contained aquatic plants. No significant changes of CO₂ concentrations were observed in control reactor at elevated CO₂ of 500, 1,000, 1500 and 2,000 ppm.

Table 2 summarizes the performance of phyto-reactors for CO₂ removal. CO₂ removal by phyto-reactors contained aquatic plants was ranged between 83-99% depending on type of aquatic plants and initial CO₂ concentrations. Increase of initial elevated CO₂

Table 2. CO₂ Utilization Rate Coefficients

Aquatic plants	Removal efficiency (%)
Control	<5
<i>C. alternifolius</i>	94-99
<i>D. fragrans</i>	94-99
<i>I. ensata</i>	87-97
<i>T. dealbata</i>	83-96

The data represents at temperature 25°C and light intensity 55 ± 5 mmole/m²/s.

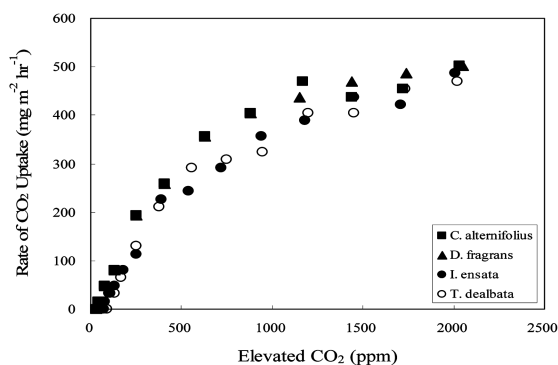


Fig. 6. Effect of initial elevated CO₂ on CO₂ utilization rate.

concentrations enhanced the CO₂ utilization rate of aquatic plants (Fig. 6). At CO₂ level of 2,000 ppm, CO₂ utilization rates of *C. alternifolius*, *D. fragrans*, *I. ensata* and *T. dealbata* were varied between 480 to 500 mg CO₂ m⁻² hr⁻¹.

4. Conclusions

The use of *C. alternifolius*, *D. fragrans*, *I. ensata* and *T. dealbata* in the PBRs were able to remove approximately 81-97% of NO₃-N and 90-98% of PO₄-P, while control reactor had comparatively lower N removal efficiency. The pH and DO in PBRs were 6.9-7.7 mg/L. and 2.7-5.8 mg/L. The rapid reduction of DO was during 2-3 days of the experiments for every PBRs contained plants. The experiments indicated that PBRs contained aquatic plants can remove CO₂ from indoor condition (500 ppm) to less than 90 ppm after 4 hrs of the experiments. Increase of elevated CO₂ concentrations of 1,000, 1,500 and 2,000 encouraged the CO₂ utilization rate in the phyto-reactors compared with ambient CO₂ level (500 ppm), CO₂ utilization rates were increased 28%, 40% and 47% for *C. alternifolius*, 30%, 44% and 52% for *D. fragrans*, 43%, 64% 76% for *I. ensata* and 40%, 58% and 69% for *T. dealbata* at initial CO₂ levels of 1,000, 1,500 and 2,000 ppm.

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